



ANNEX A5

Netheridge Cost Report

This document has been written in line with the requirements of the RAPID gate two guidance and to comply with the regulatory process pursuant to Severn Trent Water's statutory duties. The information presented relates to material or data which is still in the course of completion. Should the solution presented in this document be taken forward, Severn Trent Water will be subject to the statutory duties pursuant to the necessary consenting process, including environmental assessment and consultation as required. This document should be read with those duties in mind.



Severn Trent Water

SEVERN TRENT SOURCES STRATEGIC RESOURCE OPTIONS

Netheridge Cost Report





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Netheridge Cost Report

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ABBREVIATION AND ACRONYM LIST

Table 1 – Abbreviation and Acronym List

Abbreviation or Acronym	Meaning
ACWG	All Company Working Group
AIC	Average Incremental Cost
BAF	Biologically active filtration
BAF	Biologically active filter
CAPEX	Capital expenditure
CDR	Concept design report
GAC	Granular activated carbon
ICA	Instrumentation, Control and Automation
kWh	Kilowatt hour
MBBR	Moving Bed Biofilm Reactor
MCC	Motor control centre
MLD	Megalitres per day
N/A	Not applicable
no.	Number
NPV	Net present value
OB	Optimism Bias
OPEX	Operational expenditure
PLC	Programmable logic controller
PS	Pumping station
QCRA	Qualitative Costed Risk Assessment
RAPID	Regulator's Alliance for Progressing Infrastructure Development
SCADA	Supervisory control and data acquisition system
SRO	Strategic resource option
STS	Severn Trent sources
STW	Severn Trent Water

Abbreviation or Acronym	Meaning
UV	Ultraviolet
VAT	Value added tax
WRMP	Water Resource Management Plan
WTW	Water treatment works
WwTW	Wastewater Treatment Works

1 INTRODUCTION

1.1 CONTEXT

This Cost Report sets out the cost estimation and risk assessment carried out for the Severn Trent Sources Strategic Resource Option Netheridge (Netheridge SRO) Concept Design.

It should be read in conjunction with the Severn Trent Sources Strategic Resource Option Netheridge Concept Design Report and is part of a suite of reports completed in support of Severn Trent Water's (STW) RAPID Gate 2 Submission.

Other reports completed as part of the Gate 2 concept design development include:

- Severn Trent Source SRO - Netheridge Concept Design Report (Annex A1)
- Severn Trent Source SRO - Netheridge Process Basis of Design (Annex A3)
- Severn Trent Source SRO - Pipeline Route Appraisal Report (Annex A2) and
- Severn Trent Source SRO - Netheridge Carbon Report (Annex A4).

1.2 REPORT SCOPE

This report details the cost estimates for the Netheridge SRO and includes calculation of:

- Capital Cost estimates (Capex);
- Optimism Bias (OB);
- Qualitative Costed Risk Assessment (QCRA);
- Operational Cost Estimates (Opex);
- Net Present Value (NPV); and
- Average Incremental Cost (AIC).

1.3 GATE 2 OPTIONS

The options developed for the Netheridge SRO are as follows:

- **Option 1** - Treatment (MBBR, CoMag, Ozone, BAF, GAC) of effluent at Netheridge WwTW with transfer via 700mm dia. pipeline and discharge to the River Severn downstream of the new STT SRO Deerhurst WTW.
- **Option 2** - Treatment (MBBR, CoMag, Ozone, BAF, GAC) of effluent at Netheridge WwTW with transfer via 700mm dia. pipeline and discharge to the River Severn upstream of the gauging station at Haw Bridge.
- **Option 3** – Treatment (MBBR, CoMag, Ozone, BAF, GAC, Ion Exchange) of effluent at Netheridge WwTW with transfer via 700mm dia. pipeline and discharge to the East Channel of the River Severn downstream of the intake for Gloucester Docks.



- **Option 4** - Treatment (MBBR, CoMag, Ozone, BAF, GAC, Ion Exchange, UV) of effluent at Netheridge WwTW with transfer via 600mm dia. pipeline and discharge to direct to the G&S Canal adjacent to the Netheridge WwTW.
- **Option 5** – Additional pipeline for diversion of flows form the main STT SRO pipeline for discharge to the East Channel of the River Severn downstream of the intake for Gloucester Docks.

2 CAPITAL COSTS

2.1 CAPEX COST ESTIMATION APPROACH

2.1.1 TREATMENT PLANT UPGRADE

The treatment capital cost estimate was developed using the STW 'Cost Tool Lite' developed by Atkins/Arup, version April 2022. The STW team provided uplifts to be applied where items fell outside the limits of the cost graphs within the tool. The STW 'Cost Tool Lite' applies a Non-Standard Adjustment, as well as Internal and External Costs as On-Costs, the percentage values of those applied were provided by STW.

Severn Trent's Cost Tool Lite is an in-house tool that contains more than 20 years of historic project cost data and cost models (generated by the Severn Trent Unit Cost Analysis tool) as well as historic uplifts for prelims and client costs.

Option 5 is costed as additional to Options 1 and 2; therefore, it has been costed as the additional pipeline and the additional treatment required for discharging to this location.

2.1.2 PIPELINE

The pipeline capital cost estimate was developed using the STW 'Cost Tool Lite' developed by Atkins/Arup, version April 2022.

The lengths for the pipeline, tunnel sections and crossings were measured off the Civil 3D drawing for the pipeline route.

'Watercourse crossings' were included in the model wherever the pipeline crosses a river, stream, or land drain that is not tunnelled, this is intended to cover the additional costs incurred when crossing a watercourse.

The pipeline will require several access tracks to drain points to facilitate draining the pipeline during standby periods as outlined in the Pipeline Route Appraisal Report. Access track, and security fencing was included for access to the drain-down chambers that will be included along the length of the pipeline.

The estimated cost for the outlets were compiled using SPONS and includes the excavation (including coffer dam), concrete surround, pipework, and wall penetration for the canal outlets.

The STW 'Cost Tool Lite' developed by Atkins/Arup, version April 2022, applies a Non-Standard Adjustment, as well as Internal and External Costs as On-Costs, the percentage values applied were provided by STW.

2.2 ASSUMPTIONS

2.2.1 TREATMENT PLANT UPGRADE

The key assumptions made during completion of the Cost Tool Lite are outlined below:

- Process and connection pipeline size has been assumed.
- All electrical new equipment will be housed in one building.
- A single CoMag process stream is provided.
- For Option 5 it is assumed that Option 1 or 2 is also provided.

2.2.2 PIPELINE

The assumptions that have been made during the cost build-up of the pipeline are outlined below:

- The pipeline will be constructed using the open cut method with tunnelled sections required only for the railway, canal, and river crossings.
- Small watercourse crossings will be constructed open cut with flows managed through pumping.
- The pipeline is 700mm diameter for all open cut sections (Option 4 is 700mm dia.).
- The tunnelled sections are 1000mm diameter to facilitate construction with a 700mm pipeline within.
- All washout, air value and isolation valves are to STW standard specification.
- The outfall to the River Severn requires eel screens.
- The surge vessel has been sized without detailed surge analysis.

2.3 EXCLUSIONS

No allowance has been made for modifications required to the existing WwTW site or equipment to facilitate the construction, operation, or maintenance of the new facilities.

2.4 ON-COSTS

The on-costs applied to Capex cost build up are the STW values provided on the standard 'STW Cost Tool Lite' template PR24, there is no functionality provided on the tool to break this down further.

The on-costs applied to the treatment and the pipeline estimates differ due to the complexity of the treatment upgrade and the relative simplicity of the pipeline.

2.5 SUMMARY

Table 2-1 summarises the overall Capex costs for the five options presented in the Concept Design Report. Option 5 includes only the Capex cost of the additional treatment (ion exchange) required to discharge into the River Severn East Channel and the additional pipeline required.

All costs stated exclude the optimism bias and risk which is addressed separately in this report.

Table 2-1 – Capital Cost Summary (Excluding OB and Risk)

Option No.	Option Name	Treatment Capex	Pipeline Capex	Overall Capex Cost
Option 1	Deerhust	£69,797,800	£32,625,300	£102,423,100
Option 2	Haw Bridge	£69,797,800	£28,595,700	£98,393,500
Option 3	East Channel	£78,240,000	£9,921,500	£88,161,500
Option 4	Canal	£79,535,400	£2,421,400	£81,956,800
Option 5	SW Branch	£8,442,200	£848,600	£9,290,800

Figures have been rounded to the nearest hundred as this is the level of detail the Cost Tool Lite provides. Full spreadsheets are available in **Appendix A**.

3 RISK ASSESSMENT AND OPTIMISM BIAS

3.1 APPROACH TO RISK ASSESSMENT AND OPTIMISM BIAS

The Optimism Bias (OB) and Qualitative Costed Risk Assessment (QCRA) assessment have been carried out in accordance with the approach outlined in the Mott McDonald ACWG Cost Constituency Methodology (Rev E Feb 2022) and the Optimism Bias and Qualitative Costed Risk Assessment Template (Rev C Feb 2022).

This approach has been developed by Mott McDonald to specifically address how OB and QCRA should be assessed for water resource schemes included in the WRMPs and SRO schemes for RAPID submissions at Gates 1 and 2.

The overall approach follows the HM Treasury Green Book methodology and advocates for a reduction in optimism bias as the project risks become better understood and therefore better quantified.

3.1.1 OPTIMISM BIAS

The ACWG methodology outlines an OB process in three stages¹:

- Stage 1:** The first stage defines the project type with regard to standard and non-standard engineering project to define the upper bound of OB
- Stage 2:** The second stage scales back the OB based on the contributory factors outline in the Green Book methodology
- Stage 3:** The third stage reassess the OB based on the output of the QCRA to ensure that the OB allowance takes into account the risks that have now been costed and included separately to avoid overestimation of the OB and Risk costs.

The ACWG methodology suggests that the level of optimism bias at the conclusion of the first, second and third stages should be recorded as this will provide a point of reference for comparison across the companies.

3.1.2 QUALITATIVE COSTED RISK ASSESSMENT

The ACWG methodology for a qualitative costed risk assessment follows a typical risk assessment process with standardisation of the risk breakdown structure, risk status, likelihood estimation and impact scoring². The ACWG mythology suggests a Monte-Carlo analysis to aggregate risk with the P10, P50 and P90 risk percentiles being recorded. The P50 output from the QCRA should be used to determine the total capital cost estimates for appraisal.

¹ Refer to ACWG Cost Consistency Methodology Rev E Section 6.2.

² Refer to ACWG Cost Consistency Methodology Rev E Section 3.8.

3.2 OPTIMISM BIAS RESULTS

3.2.1 OPTIMISM BIAS SCORING SUMMARY

Based on the ACWG recommendations, the STT SRO options were split into standard and non-standard civil engineering project elements for the calculation of optimism bias; the pipeline elements are considered as standard, and the treatment elements of the project are considered as non-standard.

The options were then assessed on the confidence in the following areas: Procurement, Project Specific, Client Specific, Environment and External Influences to allow for scaling back of the upper bound of the OB based on the specifics of each option. The confidence gradings in these areas were reviewed with the Client and project team to ensure they were suitable for the current project stage.

The options underwent a final OB assessment taking into account the QCRA to give the final OB value.

Table 3-1 – Optimism Bias Summary

Option No.	Option Name	STAGE 1 Combined Upper Bound OB (%)	STAGE 2 Adjusted OB (%)	STAGE 3 Adjusted OB Inc Risk (%)
Option 1 Treatment	Deerhurst	58.96	37.10	30.49
Option 2 Treatment	Haw Bridge	59.62	37.47	30.62
Option 3	East Channel	63.58	39.65	31.41
Option 4	Canal	65.34	40.62	31.77
Option 5	SW Branch	64.02	39.89	31.50

The full analysis of optimism bias is included in Appendix B.

3.3 COSTED RISK REGISTER

The risk register has been progressed over the course of the concept design development to capture the key issues and uncertainties affecting the Netheridge scheme. There are three categories of risk: those affecting the health and safety of personnel during construction and operation, and which must be addressed as part of the CDM regulations, those affecting the construction of the project and those that impact the overall viability or scope of the project or the premise on which the project has been developed.

Risks that affect H&S, but do not have a significant impact on the overall project cost or delivery, have not been included in the QCRA. These have been identified in the Significant H&S Risk Schedule included in the Netheridge Concept Design Report.

Risks that affect the delivery of the design and construction phase of the project have been identified and appropriate cost and likelihood values were assigned to enable a Monte-Carlo analysis to be completed.

Risks that impact the overall viability or scope of the project or the premise on which the project has been developed have not been included in the QCRA, as the impact of the realisation of these risks cannot be satisfactorily quantified.

Risks in the latter category include:

- **Operating regime of the Severn to Thames Transfer SRO project changes impacting the design assumptions used for the design of the treatment process, pipeline and pump station.**

It is not possible to anticipate or quantify potential changes that may occur to the operation and requirements of the STT SRO. Given that the Netheridge scheme output is entirely dependent upon the STT SRO requirement, any changes will impact the overall design premise and project viability.

- **Changes to influent quality at Netheridge WwTW that require alteration to existing and proposed treatment processes to continue to meet consent standards.**

It is possible that changes to the influent quality at Netheridge WwTW could impact the ability of the proposed new treatment plant to meet the required STT SRO discharge consent conditions at the discharge location. For example, increase in trace metals from an industrial process in the catchment. It is not possible to quantify or cost this risk.

- **Installation of new assets at Netheridge WwTW site to meet other project needs (i.e., Gas to Grid and AMP8 Phosphorus removal) that impact on the availability of land, power, potable water and sludge handling facilities for the proposed STS SRO treatment process.**

It is understood that upgrades may occur at Netheridge WwTW in the AMP8 period. The extent and nature of these upgrades is not known but they may either utilise power, land, resources such as potable water or sludge handling, or they may render elements of the new SRO treatment process unnecessary or inappropriate. This risk cannot be costed or quantified.

- **Issues relating to access to land required for the construction of the pipeline and valve chambers, and wayleaves and easements for ongoing operation and maintenance of the pipeline.**

Options 1, 2, 3 and 5 pipelines are up to 18km long and pass-through land owned by numerous stakeholders. It is possible that the selected pipe route cannot be constructed due to issues obtaining access or wayleaves. This will be addressed fully at Gate 3 when engagement with stakeholders will be undertaken. No engagement has been undertaken at Gate 2 and so this risk cannot be quantified or costed.

3.4 RISK RESULTS

3.4.1 RISK SUMMARY

The following tables show the output from the ACWG template Risk Register and @Risk Tabs. Note that Option 5 covers the risk for the construction of the additional branch only.

Table 3-2 – Risk Values

Option No.	Option Name	P10	P50	P90
Option 1	Deerhurst	£8,107,084.06	£20,012,655.77	£34,089,166.92
Option 2	Haw Bridge	£7,731,351.65	£19,122,964.60	£32,677,017.83
Option 3	East Channel	£3,965,783.46	£12,647,664.09	£23,032,875.76
Option 4	Canal	£597,119.45	£8,196,285.07	£16,917,953.62
Option 5	SW Branch	£348,123.71	£1,261,008.16	£2,338,110.59

The full analysis of optimism bias is included in Appendix B.

3.5 SUMMARY OF CAPEX COSTS (INCLUDING OB AND RISK)

The OB value, risk value and Overall Capex cost have been summed to determine the Total Project Capex cost for each option.

Table 3-3 – Capex Cost (Including OB and Risk)

Option No.	Option Name	OB Value	Risk Value (P50)	Total Project Capex Cost
Option 1	Deerhurst	£31,228,800	£20,012,656	£153,664,600
Option 2	Haw Bridge	£30,128,100	£19,122,965	£147,644,600
Option 3	East Channel	£27,691,500	£12,647,664	£128,500,700
Option 4	Canal	£26,037,700	£8,196,285	£116,190,800
Option 5	SW Branch	£2,926,600	£1,261,008	£13,478,400

4 OPERATIONAL COST ESTIMATES

4.1 COST ESTIMATION APPROACH

The annual operating expenditure has been calculated by assessing the electrical power used on site by the equipment, the cost of labour to operate and maintain the equipment and the cost of any consumables such as chemicals and media.

4.2 ASSUMPTIONS

The basis for the estimation of the operating costs includes a number of key assumptions on the operation of the plant:

- Netheridge SRO treatment plant will treat a minimum of 20MLD on a continual basis to ensure viability of the biological treatment process.
- 35MLD of treated effluent will be pumped to the STT SRO abstraction point on 35 days of the year throughout the 80-year operational period.
- 20MLD of 'sweetening' flows to the STT SRO abstraction point will be pumped for 120 days per year.
- For the remaining 210 days per year, a sweetening flow will be provided through the SRO treatment process and will be discharged to the existing outfall.

This is a simplification of the expected operating conditions, as the number of days on which the STT SRO will call for flow over the lifetime of the project is not currently confirmed, and the treatment process flexibility to operate at a lower flowrate on days in which there is no STT SRO call for flow has not been assessed. Without further detail on the demand profile establishing how the operating costs will vary with flowrate this cannot inform the annual cost. Additionally, certain technical assumptions as part of the preliminary process design have an influence on the operating costs, for instance power costs associated with blowers are based on an estimated oxygen demand of the effluent. Consequently, the annual operating costs estimated at this stage are suitable only for the comparison of options.

Other assumptions made during build-up of the Opex cost include:

- The GAC, Ion Exchange and UV units will not operate during days that the STT SRO does not call for flow, this reduces the replacement rate of media and power consumption.
- The STT SRO will only call for flow for one period during the year.
 - It is anticipated that during the notice period prior to transfer, greater operator input will be required due to bringing process units back online, and the Opex includes additional labour for this period.
 - It is also expected that when this is complete the transfer pipeline will be drained, the Opex includes labour cost for one drain down per year.
- Operator and maintenance time are assumptions made from previous project experience and expected levels of operator input.
- For Option 5, it is assumed that 35MLD of effluent will be pumped to Haw Bridge for 35 days of the year, 20MLD of sweetening flow will be pumped for 120 days of the year and 35MLD will be provided to the East Channel for 35 days of the year.

- The cost per unit of power used was 0.20 £/kWh and labour £38.11 per hour as provided by STW.

4.3 SUMMARY

Table 4-1 summarises the overall operational costs for the five options developed during the concept design.

The treatment process accounts for most of the annual Opex costs, Option 3 and 4 treatment Opex is increased due to the additional process units.

The pipeline Opex tends to decrease with the decrease in pipe length, however there are hydraulic differences between the Option 3 and 4 discharge point that affect the power consumption – this is discussed further in the Pipeline Hydraulics Assessment report.

Option 5 shows the additional Opex cost of the SW Branch.

Table 4-1 – Operational Cost Summary

Option No.	Option Name	Treatment Opex	Pipeline Opex	Annual Opex
Option 1	Deerhurst	£1,447,915	£217,745	£1,665,660
Option 2	Haw Bridge	£1,447,915	£171,422	£1,619,337
Option 3	East Channel	£1,485,967	£90,203	£1,576,170
Option 4	Canal	£1,504,087	£92,374	£1,596,462
Option 5	SW Branch	£38,052	£180,786	£218,838

The full breakdown of Opex costs is included in Appendix C.

5 NET PRESENT VALUE & AVERAGE INCREMENTAL COST

5.1 APPROACH

To calculate the Net Present Value (NPV) the Capex costs were split out into categories based on their purpose and construction. Each category has an expected asset life associated as outlined in the All Company Working Group Mott MacDonald Cost Consistency Methodology Rev E (Feb 2022).

The asset categories and the corresponding expected asset life are outlined below:

- Process-Related Carbon Media Including GAC (4 years);
- Building Services (10 years);
- Fencing (10 years);
- ICA (Instrumentation, Control & Automation) (10 years);
- Plant and Machinery (15 years) – This has been used to represent IX resin replacement only;
- M&E (Mechanical and Electrical) Works on Pumping Stations and Treatment Works (20 years);
- Power Supply (25 years);
- Steel/Timber/GRP Structures (30 years);
- Brick/Concrete Office Structures (50 years);
- Headworks/Valves (60 years);
- Roads and Car Parks (60 years); and
- Treatment and Pumping Station Civils (incl. Intakes) (60 years).

The costs were then inputted into the Mott MacDonald NPV and AIC template (Rev C, May 2021) provided by STW. The discount factor was provided in the template, the factor used was 3.5% for years 1-30, 3% for years 31-75 and 2.5% for years 76-80 as per the Green Book recommendation.

The minimum flow used was 20MLD and the deployable output was 35MLD. The construction Capex cost was split over years 1 and 2 to represent the expected construction timeframe of c. 24 months, and Opex costs, split into fixed and variable, were shown to start from Year 3.

5.2 SUMMARY TABLES

Table 5-1 summarises the NPV and AIC outputs for the five options developed during the concept design. Note that the AIC template assumes that the WwTW flows 365 days of the year which may not be the correct operating scenario for this scheme. This scheme is anticipated to transfer 35MLD for 35 days, 20MLD for 120 days and to run on 'standby' treating 20MLD but to the existing discharge not transferring for the remainder of the year.

Note Option 5 outputs are just for the SW branch, and therefore are in addition to Option 1 or 2.



Table 5-1 – NPV and AIC Template Output

Option No.	Option Name	NPV Finance (£)		NPV Opex (£)		NPV WAFU (m ³)	AIC (p/m ³)	
		Min utilisation	Max utilisation	Min utilisation	Max utilisation		Min utilisation	Max utilisation
Option 1	Deerhurst	£168,185,540	£168,185,540	£51,419,650	£76,874,965	£263,267,297	£83.42	£93.08
Option 2	Haw Bridge	£163,915,721	£163,915,721	£49,468,463	£73,460,388	£263,267,297	£81.05	£90.17
Option 3	East Channel	£154,520,009	£154,520,009	£47,582,008	£70,083,464	£263,267,297	£76.77	£85.31
Option 4	Canal	£146,993,167	£146,993,167	£48,328,872	£71,329,031	£263,267,297	£74.19	£82.93
Option 5	SW Branch	£15,146,408	£15,146,408	£8,731,577	£15,016,144	£263,267,297	£9.07	£11.46

6 COST SUMMARY

The following Table 6-1 combines all of the costs estimates for the five Netheridge SRO options.

Table 6-1 – Cost Summary Tables

Option No.	Option Name	Capex	OB	QCRA (P50)	Total Project Capex Cost	Annual Opex	NPV Finance	NPV Opex	AIC (p/m ³)
Option 1	Deerhurst	£102,423,100	£31,228,800	£20,012,656	£153,664,600	£1,665,660	£168,185,540	£76,874,965	93.08
Option 2	Haw Bridge	£98,393,500	£30,128,100	£19,122,965	£147,644,600	£1,619,337	£163,915,721	£73,460,388	90.17
Option 3	East Channel	£88,161,500	£27,691,500	£12,647,664	£128,500,700	£1,576,170	£154,520,009	£70,083,464	85.31
Option 4	Canal	£81,956,800	£26,037,700	£8,196,285	£116,190,800	£1,596,462	£146,993,167	£71,329,031	82.93
Option 5	SW Branch	£9,290,800	£2,926,600	£1,261,008	£13,478,400	£218,838	£15,146,408	£15,016,144	11.46

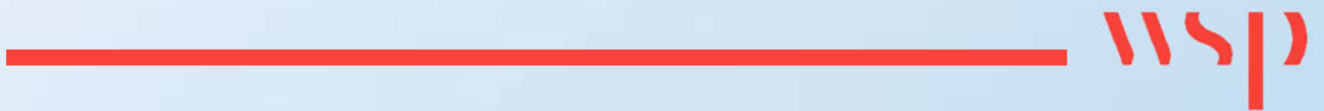
7 FUTURE WORK COST ESTIMATES

The anticipated next steps for Gate 3 and Gate 4 are outlined in the Concept Design report. The below table outlines these next steps and provides a high-level budget cost for the items of work.

	Item of Work	Cost Estimate
Gate 3	Design Development	£250,000
	Inflow flow availability review	£15,000
	Netheridge WwTW upgrades review	Inc in design development
	Advanced treatment performance pilot plant	£100,000
	Operations and Control system review and development	£15,000
	Potable water supply investigation	£7,000
	Ground investigation for pipeline & treatment site – incl. soil resistivity	£600,000
	Topographic survey for pipeline and treatment site	£75,000
	Utilities survey for treatment site	£30,000
	Pipeline LiDAR	£25,000
	Pipeline bathymetric survey	£100,000
	Discharge from drain down points	By others
	Utilities service provider engagement	By others
	Stakeholder and Landowner engagement	By others
	Environmental Surveys and reporting	By others
	Permitting Applications & consideration of permitting route	By others
	Water Resources Benefit	By others
Gate 4	Design Development	
	Permit and planning applications	
	Preparation of tender documents – incl. H&S Information	
	Land Purchase	By others

Appendix A

CAPEX COST ESTIMATE



Element Reference:
Date Issued: 19 October 2022

Notice Values are rounded

These on-cost rates may be adjusted from the default values

Rate		B&C	M&E	Mains & Sewers	Total
	Standard Cost	£ 12,868,900	£ 6,896,800	£ -	£ 19,765,700
	Non-Standard Cost	£ 32,159,900	£ 2,982,200	£ -	£ 35,142,100
0.5%	Non-Standard Adjustment	£ 64,300	£ 34,500	£ -	£ 98,800
	Construction Cost	£ 45,093,100	£ 9,913,500	£ -	£ 55,006,600
0.0%	Design Fee	£ -	£ -	£ -	£ -
	Contractor D&B Cost	£ 45,093,100	£ 9,913,500	£ -	£ 55,006,600
18.3%	Internal Costs	£ 8,238,500	£ 1,811,200	£ -	£ 10,049,700
8.6%	External Costs	£ 3,887,000	£ 854,500	£ -	£ 4,741,500
	Project Total	£ 57,218,600	£ 12,579,200	£ -	£ 69,797,800
30.5%	Optimism Bias	£ 17,446,000	£ 3,835,400	£ -	£ 21,281,400
	Business Case Cost Estimate	£ 74,664,600	£ 16,414,600	£ -	£ 91,079,200

These rates and notes may be adjusted from the standard rates
 Costs are calculated using a formula of $M \times (Quantity)^P + C$
 M is a multiplier adjuster, P is a power adjuster, C is a constant
 For Linear Cost Curves set $P = 1$
 For Unit Rate Items set $P = 1, C = 0$

Level 1	Level 2	Level 3	Level 4	Units	B&C				M&E				Mains and Sewers				Notes			
					M	P	C	Quantity	Cost	M	P	C	Quantity	Cost	M	P		C	Quantity	Cost
NON-INFRA	Sewage Treatment	Chem Dosing	P Removal	m3	76,090	0	0	120 m3	£ 153,496	172,940	0	0	120 m3	£ 353,493	0	0	0	m3	#VALUE!	Ferrous Sulphite
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	330 kW	£ 770,868	17,996	1	0	150 kW	£ 420,550					£ -	MBBR PS
NON-INFRA	Sewage Treatment	Chem Dosing	P Removal	m3	76,090	0	0	60 m3	£ 138,666	172,940	0	0	60 m3	£ 318,734					£ -	Ferric Sulphate
NON-INFRA	Sludge Treatment	Sludge Holding Tank	Sludge Holding Tank	m3	1,538	1	0	475 m3	£ 102,767	19,179	0	0	475 m3	£ 244,095					£ -	
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	165 kW	£ 526,172	17,996	1	0	150 kW	£ 420,550					£ -	SPS Wet Well & Pumps Ozone
NON-INFRA	Water Treatment	GAC	GAC , RGF Type	m3	4,260	1	0	1,132 m3	£ 4,822,794	3,057	1	0	m3	#VALUE!					£ -	BAFF Tank
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	165 kW	£ 526,172	17,996	1	0	150 kW	£ 420,550					£ -	BAFF PS
NON-INFRA	Water Treatment	GAC	GAC , RGF Type	m3	4,260	1	0	1,056 m3	£ 4,499,002	3,057	1	0	1,056 m3	£ 3,228,311					£ -	
NON-INFRA	Water Treatment	Chlorination	Chlorination Dosing	kg/d	9,591	1	0	2 kg/d	£ 15,178	178,910	0	0	2 kg/d	£ 203,484					£ -	
NON-INFRA	Sludge Treatment	Sludge Holding Tank	Sludge Holding Tank	m3	1,538	1	0	142 m3	£ 45,115	19,179	0	0	142 m3	£ 148,295					£ -	Thickened Sludge Tank
NON-INFRA	Sludge Treatment	Sludge Pumping	Sludge Pumping	kW					£ -	35,373	1	0	19 kW	£ 186,443					£ -	Sludge Thickener Feed Pumps
FREE ENTRY	Sludge Treatment	No	Sludge Thickener Drum & Belt		75,838	#N/A	#N/A	1	£ 75,838	390,284	#N/A	#N/A	1	£ 390,284					£ -	Sludge Thickener Drum & Belt
NON-INFRA	Sludge Treatment	Sludge Pumping	Sludge Pumping	kW					£ -	35,373	1	0	8 kW	£ 115,648					£ -	Thickened Sludge Pumps
FREE ENTRY	Outlet to River	No	Outlet		145,000	#N/A	#N/A	1	£ 145,000					£ -					£ -	Outlet
FREE ENTRY	MBBR	No	MBBR		#####	#N/A	#N/A	1	£ 11,353,500					£ -					£ -	MBBR
FREE ENTRY	Comag	No	Comag		3,327,198	#N/A	#N/A	1	£ 3,327,198					£ -					£ -	Comag
FREE ENTRY	BAFF M&E	No	BAFF M&E						£ -	2,175,000	#N/A	#N/A	1	£ 2,175,000					£ -	BAFF M&E
NON-STANDARD	Site wide SCADA / control system	No.	x	No.	27,783	1	0	522 No.	£ 14,502,465	27,783	1	0	No.	#VALUE!					£ -	
FREE ENTRY	Ozone Curve	No	Ozone		2,755,902	#N/A	#N/A	1	£ 2,755,902					£ -					£ -	Ozone
FREE ENTRY	Interstage Pumps	No	Uplift oor						£ -	164,503	#N/A	#N/A	1	£ 164,503					£ -	Uplift oor
FREE ENTRY	Ferrous Dosing	No	Uplift oor						£ -	252,438	#N/A	#N/A	1	£ 252,438					£ -	Uplift oor
NON-INFRA	Water Treatment	Poly Dosing	Poly Dosing	kg/d	24,995	0	0	28 kg/d	£ 79,430	343,823	0	0	28 kg/d	£ 479,789					£ -	CoMag Poly dosing
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	206 kW	£ 594,607	17,996	1	0	69 kW	£ 258,053					£ -	Clean backwash
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	206 kW	£ 594,607	17,996	1	0	15 kW	£ 98,825					£ -	Dirty backwash

Element Reference:
Date Issued: 19 October 2022

Notice Values are rounded

These on-cost rates may be adjusted from the default values

Rate		B&C	M&E	Mains & Sewers	Total
	Standard Cost	£ 12,868,900	£ 6,896,800	£ -	£ 19,765,700
	Non-Standard Cost	£ 32,159,900	£ 2,982,200	£ -	£ 35,142,100
0.5%	Non-Standard Adjustment	£ 64,300	£ 34,500	£ -	£ 98,800
	Construction Cost	£ 45,093,100	£ 9,913,500	£ -	£ 55,006,600
0.0%	Design Fee	£ -	£ -	£ -	£ -
	Contractor D&B Cost	£ 45,093,100	£ 9,913,500	£ -	£ 55,006,600
18.3%	Internal Costs	£ 8,238,500	£ 1,811,200	£ -	£ 10,049,700
8.6%	External Costs	£ 3,887,000	£ 854,500	£ -	£ 4,741,500
	Project Total	£ 57,218,600	£ 12,579,200	£ -	£ 69,797,800
30.6%	Optimism Bias	£ 17,520,300	£ 3,851,800	£ -	£ 21,372,100
	Business Case Cost Estimate	£ 74,738,900	£ 16,431,000	£ -	£ 91,169,900

These rates and notes may be adjusted from the standard rates
 Costs are calculated using a formula of $M \times (Quantity)^P + C$
 M is a multiplier adjuster, P is a power adjuster, C is a constant
 For Linear Cost Curves set $P = 1$
 For Unit Rate Items set $P = 1, C = 0$

Level 1	Level 2	Level 3	Level 4	Units	B&C				M&E				Mains and Sewers				Notes			
					M	P	C	Quantity	Cost	M	P	C	Quantity	Cost	M	P		C	Quantity	Cost
NON-INFRA	Sewage Treatment	Chem Dosing	P Removal	m3	76,090	0	0	120 m3	£ 153,496	172,940	0	0	120 m3	£ 353,493	0	0	0	m3	#VALUE!	Ferrous Sulphite
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	330 kW	£ 770,868	17,996	1	0	150 kW	£ 420,550					£ -	MBBR PS
NON-INFRA	Sewage Treatment	Chem Dosing	P Removal	m3	76,090	0	0	60 m3	£ 138,666	172,940	0	0	60 m3	£ 318,734					£ -	Ferric Sulphate
NON-INFRA	Sludge Treatment	Sludge Holding Tank	Sludge Holding Tank	m3	1,538	1	0	475 m3	£ 102,767	19,179	0	0	475 m3	£ 244,095					£ -	
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	165 kW	£ 526,172	17,996	1	0	150 kW	£ 420,550					£ -	SPS Wet Well & Pumps Ozone
NON-INFRA	Water Treatment	GAC	GAC , RGF Type	m3	4,260	1	0	1,132 m3	£ 4,822,794	3,057	1	0	m3	#VALUE!					£ -	BAFF Tank
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	165 kW	£ 526,172	17,996	1	0	150 kW	£ 420,550					£ -	BAFF PS
NON-INFRA	Water Treatment	GAC	GAC , RGF Type	m3	4,260	1	0	1,056 m3	£ 4,499,002	3,057	1	0	1,056 m3	£ 3,228,311					£ -	
NON-INFRA	Water Treatment	Chlorination	Chlorination Dosing	kg/d	9,591	1	0	2 kg/d	£ 15,178	178,910	0	0	2 kg/d	£ 203,484					£ -	
NON-INFRA	Sludge Treatment	Sludge Holding Tank	Sludge Holding Tank	m3	1,538	1	0	142 m3	£ 45,115	19,179	0	0	142 m3	£ 148,295					£ -	Thickened Sludge Tank
NON-INFRA	Sludge Treatment	Sludge Pumping	Sludge Pumping	kW					£ -	35,373	1	0	19 kW	£ 186,443					£ -	Sludge Thickener Feed Pumps
FREE ENTRY	Sludge Treatment	No	Sludge Thickener Drum & Belt		75,838	#N/A	#N/A	1	£ 75,838	390,284	#N/A	#N/A	1	£ 390,284					£ -	Sludge Thickener Drum & Belt
NON-INFRA	Sludge Treatment	Sludge Pumping	Sludge Pumping	kW					£ -	35,373	1	0	8 kW	£ 115,648					£ -	Thickened Sludge Pumps
FREE ENTRY	Outlet to River	No	Outlet		145,000	#N/A	#N/A	1	£ 145,000					£ -					£ -	Outlet
FREE ENTRY	MBBR	No	MBBR		#####	#N/A	#N/A	1	£ 11,353,500					£ -					£ -	MBBR
FREE ENTRY	Comag	No	Comag		3,327,198	#N/A	#N/A	1	£ 3,327,198					£ -					£ -	Comag
FREE ENTRY	BAFF M&E	No	BAFF M&E						£ -	2,175,000	#N/A	#N/A	1	£ 2,175,000					£ -	BAFF M&E
NON-STANDARD	Site wide SCADA / control system	No.	x	No.	27,783	1	0	522 No.	£ 14,502,465	27,783	1	0	No.	#VALUE!					£ -	
FREE ENTRY	Ozone Curve	No	Ozone		2,755,902	#N/A	#N/A	1	£ 2,755,902					£ -					£ -	Ozone
FREE ENTRY	Interstage Pumps	No	Uplift oor						£ -	164,503	#N/A	#N/A	1	£ 164,503					£ -	Uplift oor
FREE ENTRY	Ferrous Dosing	No	Uplift oor						£ -	252,438	#N/A	#N/A	1	£ 252,438					£ -	Uplift oor
NON-INFRA	Water Treatment	Poly Dosing	Poly Dosing	kg/d	24,995	0	0	28 kg/d	£ 79,430	343,823	0	0	28 kg/d	£ 479,789					£ -	CoMag Poly dosing
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	206 kW	£ 594,607	17,996	1	0	69 kW	£ 258,053					£ -	Clean backwash
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	206 kW	£ 594,607	17,996	1	0	15 kW	£ 98,825					£ -	Dirty backwash

Element Reference:
Date Issued: 19 October 2022

Notice Values are rounded

These on-cost rates may be adjusted from the default values

Rate		B&C	M&E	Mains & Sewers	Total
	Standard Cost	£ 13,395,000	£ 7,317,400	£ -	£ 20,712,400
	Non-Standard Cost	£ 33,935,100	£ 6,908,600	£ -	£ 40,843,700
0.5%	Non-Standard Adjustment	£ 67,000	£ 36,600	£ -	£ 103,600
	Construction Cost	£ 47,397,100	£ 14,262,600	£ -	£ 61,659,700
0.0%	Design Fee	£ -	£ -	£ -	£ -
	Contractor D&B Cost	£ 47,397,100	£ 14,262,600	£ -	£ 61,659,700
18.3%	Internal Costs	£ 8,659,500	£ 2,605,800	£ -	£ 11,265,300
8.6%	External Costs	£ 4,085,600	£ 1,229,400	£ -	£ 5,315,000
	Project Total	£ 60,142,200	£ 18,097,800	£ -	£ 78,240,000
31.4%	Optimism Bias	£ 18,890,700	£ 5,684,500	£ -	£ 24,575,200
	Business Case Cost Estimate	£ 79,032,900	£ 23,782,300	£ -	£ 102,815,200

These rates and notes may be adjusted from the standard rates
 Costs are calculated using a formula of $M \times (\text{Quantity})^P + C$
 M is a multiplier adjuster, P is a power adjuster, C is a constant
 For Linear Cost Curves set P = 1
 For Unit Rate Items set P = 1, C = 0

Level 1	Level 2	Level 3	Level 4	Units	B&C				M&E				Mains and Sewers				Notes			
					M	P	C	Quantity	Cost	M	P	C	Quantity	Cost	M	P		C	Quantity	Cost
NON-INFRA	Sewage Treatment	Chem Dosing	P Removal	m3	76,090	0	0	120 m3	£ 153,496	172,940	0	0	120 m3	£ 353,493	0	0	0	m3	#VALUE!	Ferrous Sulphite
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	330 kW	£ 770,868	17,996	1	0	150 kW	£ 420,550					£ -	MBBR PS
NON-INFRA	Sewage Treatment	Chem Dosing	P Removal	m3	76,090	0	0	60 m3	£ 138,666	172,940	0	0	60 m3	£ 318,734					£ -	Ferric Sulphate
NON-INFRA	Sludge Treatment	Sludge Holding Tank	Sludge Holding Tank	m3	1,538	1	0	475 m3	£ 102,767	19,179	0	0	475 m3	£ 244,095					£ -	
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	165 kW	£ 526,172	17,996	1	0	150 kW	£ 420,550					£ -	SPS Wet Well & Pumps Ozone
NON-INFRA	Water Treatment	GAC	GAC , RGF Type	m3	4,260	1	0	1,132 m3	£ 4,822,794	3,057	1	0	m3	#VALUE!					£ -	BAFF Tank
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	165 kW	£ 526,172	17,996	1	0	150 kW	£ 420,550					£ -	BAFF PS
NON-INFRA	Water Treatment	GAC	GAC , RGF Type	m3	4,260	1	0	1,056 m3	£ 4,499,002	3,057	1	0	1,056 m3	£ 3,228,311					£ -	
NON-INFRA	Water Treatment	Chlorination	Chlorination Dosing	kg/d	9,591	1	0	2 kg/d	£ 15,178	178,910	0	0	2 kg/d	£ 203,484					£ -	
NON-INFRA	Sludge Treatment	Sludge Holding Tank	Sludge Holding Tank	m3	1,538	1	0	142 m3	£ 45,115	19,179	0	0	142 m3	£ 148,295					£ -	Thickened Sludge Tank
NON-INFRA	Sludge Treatment	Sludge Pumping	Sludge Pumping	kW					£ -	35,373	1	0	19 kW	£ 186,443					£ -	Sludge Thickener Feed Pumps
FREE ENTRY	Sludge Treatment	No	Sludge Thickener Drum & Belt		75,838	#N/A	#N/A	1	£ 75,838	390,284	#N/A	#N/A	1	£ 390,284					£ -	Sludge Thickener Drum & Belt
NON-INFRA	Sludge Treatment	Sludge Pumping	Sludge Pumping	kW					£ -	35,373	1	0	8 kW	£ 115,648					£ -	Thickened Sludge Pumps
FREE ENTRY	Outlet to River	No	Outlet		145,000	#N/A	#N/A	1	£ 145,000					£ -					£ -	Outlet
FREE ENTRY	MBBR	No	MBBR		#####	#N/A	#N/A	1	£ 11,353,500					£ -					£ -	MBBR
FREE ENTRY	Comag	No	Comag		3,327,198	#N/A	#N/A	1	£ 3,327,198					£ -					£ -	Comag
FREE ENTRY	BAFF M&E	No	BAFF M&E						£ -	2,175,000	#N/A	#N/A	1	£ 2,175,000					£ -	BAFF M&E
NON-STANDARD	Site wide SCADA / control system	No.	x	No.	27,783	1	0	522 No.	£ 14,502,465	27,783	1	0	No.	#VALUE!					£ -	
FREE ENTRY	Ozone Curve	No	Ozone		2,755,902	#N/A	#N/A	1	£ 2,755,902					£ -					£ -	Ozone
FREE ENTRY	Interstage Pumps	No	Uplift oor						£ -	164,503	#N/A	#N/A	1	£ 164,503					£ -	Uplift oor
FREE ENTRY	Ferrous Dosing	No	Uplift oor						£ -	252,438	#N/A	#N/A	1	£ 252,438					£ -	Uplift oor
NON-INFRA	Water Treatment	Poly Dosing	Poly Dosing	kg/d	24,995	0	0	28 kg/d	£ 79,430	343,823	0	0	28 kg/d	£ 479,789					£ -	CoMag Poly dosing
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	206 kW	£ 594,607	17,996	1	0	69 kW	£ 258,053					£ -	Clean backwash
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	206 kW	£ 594,607	17,996	1	0	15 kW	£ 98,825					£ -	Dirty backwash
FREE ENTRY	ITEM DESCRIPTION	ITEM UNITS	OTHER DETAILS		1,775,152	#N/A	#N/A	1	£ 1,775,152	2,610,651	#N/A	#N/A	1	£ 2,610,651					£ -	Ion Exchange
FREE ENTRY	ITEM DESCRIPTION	ITEM UNITS	IX Uplift						£ -	1,315,741	#N/A	#N/A	1	£ 1,315,741					£ -	Uplift oor
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	165 kW	£ 526,172	17,996	1	0	150 kW	£ 420,550					£ -	IX Lift PS

Element Reference:
Date Issued: 19 October 2022

Notice Values are rounded

These on-cost rates may be adjusted from the default values

Rate		B&C	M&E	Mains & Sewers	Total
	Standard Cost	£ 13,395,000	£ 7,317,400	£ -	£ 20,712,400
	Non-Standard Cost	£ 34,114,100	£ 7,750,400	£ -	£ 41,864,500
0.5%	Non-Standard Adjustment	£ 67,000	£ 36,600	£ -	£ 103,600
	Construction Cost	£ 47,576,100	£ 15,104,400	£ -	£ 62,680,500
0.0%	Design Fee	£ -	£ -	£ -	£ -
	Contractor D&B Cost	£ 47,576,100	£ 15,104,400	£ -	£ 62,680,500
18.3%	Internal Costs	£ 8,692,200	£ 2,759,600	£ -	£ 11,451,800
8.6%	External Costs	£ 4,101,100	£ 1,302,000	£ -	£ 5,403,100
	Project Total	£ 60,369,400	£ 19,166,000	£ -	£ 79,535,400
31.8%	Optimism Bias	£ 19,179,400	£ 6,089,000	£ -	£ 25,268,400
	Business Case Cost Estimate	£ 79,548,800	£ 25,255,000	£ -	£ 104,803,800

These rates and notes may be adjusted from the standard rates

Costs are calculated using a formula of $M \times (Quantity)^P + C$

M is a multiplier adjuster, P is a power adjuster, C is a constant

For Linear Cost Curves set P = 1

For Unit Rate Items set P = 1, C = 0

Level 1	Level 2	Level 3	Level 4	Units	B&C				M&E				Mains and Sewers				Notes			
					M	P	C	Quantity	Cost	M	P	C	Quantity	Cost	M	P		C	Quantity	Cost
NON-INFRA	Sewage Treatment	Chem Dosing	P Removal	m3	76,090	0	0	120 m3	£ 153,496	172,940	0	0	120 m3	£ 353,493	0	0	0	m3	#VALUE!	Ferrous Sulphite
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	330 kW	£ 770,868	17,996	1	0	150 kW	£ 420,550					£ -	MBBR PS
NON-INFRA	Sewage Treatment	Chem Dosing	P Removal	m3	76,090	0	0	60 m3	£ 138,666	172,940	0	0	60 m3	£ 318,734					£ -	Ferric Sulphate
NON-INFRA	Sludge Treatment	Sludge Holding Tank	Sludge Holding Tank	m3	1,538	1	0	475 m3	£ 102,767	19,179	0	0	475 m3	£ 244,095					£ -	
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	165 kW	£ 526,172	17,996	1	0	150 kW	£ 420,550					£ -	SPS Wet Well & Pumps Ozone
NON-INFRA	Water Treatment	GAC	GAC , RGF Type	m3	4,260	1	0	1,132 m3	£ 4,822,794	3,057	1	0	m3	#VALUE!					£ -	BAFF Tank
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	165 kW	£ 526,172	17,996	1	0	150 kW	£ 420,550					£ -	BAFF PS
NON-INFRA	Water Treatment	GAC	GAC , RGF Type	m3	4,260	1	0	1,056 m3	£ 4,499,002	3,057	1	0	1,056 m3	£ 3,228,311					£ -	
NON-INFRA	Water Treatment	Chlorination	Chlorination Dosing	kg/d	9,591	1	0	2 kg/d	£ 15,178	178,910	0	0	2 kg/d	£ 203,484					£ -	
NON-INFRA	Sludge Treatment	Sludge Holding Tank	Sludge Holding Tank	m3	1,538	1	0	142 m3	£ 45,115	19,179	0	0	142 m3	£ 148,295					£ -	Thickened Sludge Tank
NON-INFRA	Sludge Treatment	Sludge Pumping	Sludge Pumping	kW					£ -	35,373	1	0	19 kW	£ 186,443					£ -	Sludge Thickener Feed Pumps
FREE ENTRY	Sludge Treatment	No	Sludge Thickener Drum & Belt		75,838	#N/A	#N/A	1	£ 75,838	390,284	#N/A	#N/A	1	£ 390,284					£ -	Sludge Thickener Drum & Belt
NON-INFRA	Sludge Treatment	Sludge Pumping	Sludge Pumping	kW					£ -	35,373	1	0	8 kW	£ 115,648					£ -	Thickened Sludge Pumps
FREE ENTRY	Outlet to River	No	Outlet		145,000	#N/A	#N/A	1	£ 145,000					£ -					£ -	Outlet
FREE ENTRY	MBBR	No	MBBR		#####	#N/A	#N/A	1	£ 11,353,500					£ -					£ -	MBBR
FREE ENTRY	Comag	No	Comag		3,327,198	#N/A	#N/A	1	£ 3,327,198					£ -					£ -	Comag
FREE ENTRY	BAFF M&E	No	BAFF M&E						£ -	2,175,000	#N/A	#N/A	1	£ 2,175,000					£ -	BAFF M&E
NON-STANDARD	Site wide SCADA / control system	No.	x	No.	27,783	1	0	522 No.	£ 14,502,465	27,783	1	0	No.	#VALUE!					£ -	
FREE ENTRY	Ozone Curve	No	Ozone		2,755,902	#N/A	#N/A	1	£ 2,755,902					£ -					£ -	Ozone
FREE ENTRY	Interstage Pumps	No	Uplift oor						£ -	164,503	#N/A	#N/A	1	£ 164,503					£ -	Uplift oor
FREE ENTRY	Ferrous Dosing	No	Uplift oor						£ -	252,438	#N/A	#N/A	1	£ 252,438					£ -	Uplift oor
NON-INFRA	Water Treatment	Poly Dosing	Poly Dosing	kg/d	24,995	0	0	28 kg/d	£ 79,430	343,823	0	0	28 kg/d	£ 479,789					£ -	CoMag Poly dosing
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	206 kW	£ 594,607	17,996	1	0	69 kW	£ 258,053					£ -	Clean backwash
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	206 kW	£ 594,607	17,996	1	0	15 kW	£ 98,825					£ -	Dirty backwash
FREE ENTRY	ITEM DESCRIPTION	ITEM UNITS	OTHER DETAILS		1,775,152	#N/A	#N/A	1	£ 1,775,152	2,610,651	#N/A	#N/A	1	£ 2,610,651					£ -	Ion Exchange
FREE ENTRY	ITEM DESCRIPTION	ITEM UNITS	IX Uplift						£ -	1,315,741	#N/A	#N/A	1	£ 1,315,741					£ -	Uplift oor
NON-INFRA	Sewage Treatment	Interstage Pumping	Interstage Pumping	kW	31,579	1	0	165 kW	£ 526,172	17,996	1	0	150 kW	£ 420,550					£ -	IX Lift PS
FREE ENTRY	ITEM DESCRIPTION	ITEM UNITS	OTHER DETAILS		179,055	#N/A	#N/A	1	£ 179,055	501,504	#N/A	#N/A	1	£ 501,504					£ -	UV
FREE ENTRY	ITEM DESCRIPTION	ITEM UNITS	UV uplift			#N/A	#N/A		#VALUE!	340,279	#N/A	#N/A	1	£ 340,279		#N/A	#N/A		#VALUE!	Uplift oor

Element Reference:
Date Issued: 19 October 2022

Notice Values are rounded

These on-cost rates may be adjusted from the default values

Rate		B&C	M&E	Mains & Sewers	Total
	Standard Cost	£ 1,217,300	£ 1,398,600	£ 16,250,900	£ 18,866,800
	Non-Standard Cost	£ 853,700	£ -	£ 1,567,800	£ 2,421,500
19.3%	Non-Standard Adjustment	£ 234,900	£ 269,900	£ 3,136,400	£ 3,641,200
	Construction Cost	£ 2,305,900	£ 1,668,500	£ 20,955,100	£ 24,929,500
0.0%	Design Fee	£ -	£ -	£ -	£ -
	Contractor D&B Cost	£ 2,305,900	£ 1,668,500	£ 20,955,100	£ 24,929,500
12.8%	Internal Costs	£ 294,900	£ 213,400	£ 2,680,200	£ 3,188,500
18.1%	External Costs	£ 416,900	£ 301,700	£ 3,788,700	£ 4,507,300
	Project Total	£ 3,017,700	£ 2,183,600	£ 27,424,000	£ 32,625,300
30.5%	Optimism Bias	£ 920,100	£ 665,800	£ 8,361,600	£ 9,947,500
	Business Case Cost Estimate	£ 3,937,800	£ 2,849,400	£ 35,785,600	£ 42,572,800

These rates and notes may be adjusted from the standard rates
 Costs are calculated using a formula of $M \times (Quantity)^P + C$
 M is a multiplier adjuster, P is a power adjuster, C is a constant
 For Linear Cost Curves set P = 1
 For Unit Rate Items set P = 1, C = 0

Level 1	Level 2	Level 3	Level 4	Units	B&C				M&E				Mains and Sewers				Notes			
					M	P	C	Quantity	Cost	M	P	C	Quantity	Cost	M	P		C	Quantity	Cost
INFRA	Distribution	Pressure Mains in Rural/Suburban Highway	Diameter: 700mm	m															Includes 650m from Transfer PS to pipeline Ch 0	
INFRA	Distribution	Pressure Mains in Field / Verges	Diameter: 700mm	m	0		0	m	#VALUE!	0		0	m	#VALUE!	772	1	11,113	17,750 m	£ 13,722,163	
INFRA	Distribution	Tunnelling / Pipejacking	Diameter: 1200mm	m	0		0	m	#VALUE!	0		0	m	#VALUE!	4,223	1	0	450 m	£ 1,900,405	
NON-STANDARD	PIPELINE EXTRA OVERS	CROSSINGS	Watercourse crossings	Nr											55,565	1	0	24 Nr	£ 1,333,560	
																		1		
NON-STANDARD	PIPELINE EXTRA OVERS	CROSSINGS	Overhead Electric Crossings (Pylons supported)	Nr											11,113	1	0	20 Nr	£ 222,260	
																		9		
																		1		
																		1		
NON-STANDARD	PERMANENT SITE WORKS	ACCESS	Access Track	m	4,137	1	0	2,400 m	£ 441,400										£ -	
NON-INFRA	Distribution	Surge Vessel	Surge Vessel	m3	8,577	0	0	50 m3	£ 33,407	67,007	0	0	50 m3	£ 271,650					£ -	
NON-STANDARD	PERMANENT SITE WORKS	PERMANENT SITE FEATURES	Security fencing	m	78	1	0	400 m	£ 31,116										£ -	
FREE ENTRY	Submerged Outlet	Item	Submerged Outlet						£ -						12,000	#N/A	#N/A	1	£ 12,000	Submerged Outlet
NON-STANDARD	OTHERS	WORK ON EXISTING MAINS	Installation of new pumping station on existing main	Nr	38,896	1	0	8 Nr	£ 311,164										£ -	Pump chambers to drain down pipeline
FREE ENTRY	Eel screen	ITEM UNITS	OTHER DETAILS		50,000	#N/A	#N/A	1	£ 50,000										£ -	Eel weir chamber and flow metering
FREE ENTRY	Hydraulic Break	ITEM UNITS	OTHER DETAILS		20,000	#N/A	#N/A	1	£ 20,000										#VALUE!	Hydraulic break chamber
NON-INFRA	Water Treatment	Major Water Pumping Station	Major Water Pumping	kW	31,579	1	0	719 kW	£ 1,183,913	17,996	1	0	719 kW	£ 1,126,951					£ -	Transfer Lift PS

Element Reference:
Date Issued: 19 October 2022

Notice Values are rounded

These on-cost rates may be adjusted from the default values

Rate		B&C	M&E	Mains & Sewers	Total
	Standard Cost	£ 1,089,200	£ 1,260,400	£ 14,203,900	£ 16,553,500
	Non-Standard Cost	£ 959,700	£ -	£ 1,142,400	£ 2,102,100
19.3%	Non-Standard Adjustment	£ 210,200	£ 243,300	£ 2,741,400	£ 3,194,900
	Construction Cost	£ 2,259,100	£ 1,503,700	£ 18,087,700	£ 21,850,500
0.0%	Design Fee	£ -	£ -	£ -	£ -
	Contractor D&B Cost	£ 2,259,100	£ 1,503,700	£ 18,087,700	£ 21,850,500
12.8%	Internal Costs	£ 288,900	£ 192,300	£ 2,313,400	£ 2,794,600
18.1%	External Costs	£ 408,400	£ 271,900	£ 3,270,300	£ 3,950,600
	Project Total	£ 2,956,400	£ 1,967,900	£ 23,671,400	£ 28,595,700
30.6%	Optimism Bias	£ 905,200	£ 602,600	£ 7,248,200	£ 8,756,000
	Business Case Cost Estimate	£ 3,861,600	£ 2,570,500	£ 30,919,600	£ 37,351,700

These rates and notes may be adjusted from the standard rates
 Costs are calculated using a formula of $M \times (\text{Quantity})^P + C$
 M is a multiplier adjuster, P is a power adjuster, C is a constant
 For Linear Cost Curves set $P = 1$
 For Unit Rate Items set $P = 1, C = 0$

Level 1	Level 2	Level 3	Level 4	Units	B&C					M&E					Mains and Sewers					Notes
					M	P	C	Quantity	Cost	M	P	C	Quantity	Cost	M	P	C	Quantity	Cost	
INFRA	Distribution	Pressure Mains in Rural/Suburban Highway	Diameter: 700mm	m					£ -						950	1	11,113	650 m	£ 628,328	Includes 650m from Transfer PS to pipeline Ch 0
INFRA	Distribution	Pressure Mains in Field / Verges	Diameter: 700mm	m	0		0	m	#VALUE!	0		0	m	#VALUE!	772	1	11,113	15,100 m	£ 11,675,161	
INFRA	Distribution	Tunnelling / Pipejacking	Diameter: 1200mm	m	0		0	m	#VALUE!	0		0	m	#VALUE!	4,223	1	0	450 m	£ 1,900,405	
NON-STANDARD	PIPELINE EXTRA OVERS	CROSSINGS	Watercourse crossings	Nr					£ -						55,565	1	0	16 Nr	£ 889,040	
NON-STANDARD	PIPELINE EXTRA OVERS	CROSSINGS	Overhead Electric Crossings (Pylons supported)	Nr					£ -						11,113	1	0	12 Nr	£ 133,356	
NON-STANDARD	PERMANENT SITE WORKS	ACCESS	Access Track	m	4,137	1	0	3,000 m	£ 504,637										£ -	Assuming 9 chambers
NON-INFRA	Distribution	Surge Vessel	Surge Vessel	m3	8,577	0	0	50 m3	£ 33,407	67,007	0	0	50 m3	£ 271,650					£ -	
NON-STANDARD	PERMANENT SITE WORKS	PERMANENT SITE FEATURES	Security fencing	m	78	1	0	450 m	£ 35,006										£ -	Assuming 9 chambers
FREE ENTRY	Submerged Outlet	item	Submerged Outlet						£ -						120,000	#N/A	#N/A	1	£ 120,000	Submerged Outlet
NON-STANDARD	OTHERS	WORK ON EXISTING MAINS	Installation of new pumping station on existing main	Nr	38,896	1	0	9 Nr	£ 350,060										£ -	Pump chambers to drain down pipeline
FREE ENTRY	ITEM DESCRIPTION	ITEM UNITS	OTHER DETAILS		50,000	#N/A	#N/A	1	£ 50,000										£ -	Eel Weir Chamber and Flow Metering
FREE ENTRY	ITEM DESCRIPTION	ITEM UNITS	OTHER DETAILS		20,000	#N/A	#N/A	1	£ 20,000										#VALUE!	Hydraulic break chamber
NON-INFRA	Water Treatment	Major Water Pumping Station	Major Water Pumping	kW	31,579	1	0	584 kW	£ 1,055,747	17,996	1	0	584 kW	£ 988,782					£ -	Transfer Lift PS

Element Reference:
Date Issued: 19 October 2022

Notice Values are rounded

These on-cost rates may be adjusted from the default values

Rate		B&C	M&E	Mains & Sewers	Total
	Standard Cost	£ 504,500	£ 665,200	£ 195,700	£ 1,365,400
	Non-Standard Cost	£ 221,200	£ -	£ -	£ 221,200
19.3%	Non-Standard Adjustment	£ 97,400	£ 128,400	£ 37,800	£ 263,600
	Construction Cost	£ 823,100	£ 793,600	£ 233,500	£ 1,850,200
0.0%	Design Fee	£ -	£ -	£ -	£ -
	Contractor D&B Cost	£ 823,100	£ 793,600	£ 233,500	£ 1,850,200
12.8%	Internal Costs	£ 105,300	£ 101,500	£ 29,900	£ 236,700
18.1%	External Costs	£ 148,800	£ 143,500	£ 42,200	£ 334,500
	Project Total	£ 1,077,200	£ 1,038,600	£ 305,600	£ 2,421,400
31.8%	Optimism Bias	£ 342,200	£ 330,000	£ 97,100	£ 769,300
	Business Case Cost Estimate	£ 1,419,400	£ 1,368,600	£ 402,700	£ 3,190,700

These rates and notes may be adjusted from the standard rates
 Costs are calculated using a formula of $M \times (Quantity)^P + C$
 M is a multiplier adjuster, P is a power adjuster, C is a constant
 For Linear Cost Curves set $P = 1$
 For Unit Rate Items set $P = 1, C = 0$

Level 1	Level 2	Level 3	Level 4	Units	B&C					M&E					Mains and Sewers					Notes	
					M	P	C	Quantity	Cost	M	P	C	Quantity	Cost	M	P	C	Quantity	Cost		
INFRA	Distribution	Pressure Mains in Field / Verges	Diameter: 600mm	m					£ -							391	1	0	500 m	£ 195,745	
NON-STANDARD	PERMANENT SITE WORKS	ACCESS	Access Track	m	4,137	1	0	200 m	£ 99,386	0		0	m	#VALUE!						£ -	
NON-STANDARD						#N/A	#N/A		#VALUE!		#N/A	#N/A		#VALUE!		#N/A	#N/A		#VALUE!		
NON-INFRA	Distribution	Surge Vessel	Surge Vessel	m3	8,577	0	0	50 m3	£ 33,407	67,007	0	0	50 m3	£ 271,650						£ -	
NON-STANDARD	PERMANENT SITE WORKS	PERMANENT SITE FEATURES	Security fencing	m	78	1	0	280 m	£ 21,781					£ -						£ -	
FREE ENTRY	ITEM DESCRIPTION	ITEM UNITS	OTHER DETAILS		50,000	#N/A	#N/A	1	£ 50,000					£ -						£ -	Outlet will be through the existing canal wall
FREE ENTRY	ITEM DESCRIPTION	ITEM UNITS	OTHER DETAILS		50,000	#N/A	#N/A	1	£ 50,000		#N/A	#N/A		#VALUE!		#N/A	#N/A		#VALUE!		Eel Weir Chamber and Flow Metering
NON-INFRA	Water Treatment	Major Water Pumping Station	Major Water Pumping	kW	31,579	1	0	135 kW	£ 471,099	17,996	1	0	135 kW	£ 393,585						£ -	Transfer Lift PS

Element Reference:
Date Issued: 19 October 2022

Notice Values are rounded

These on-cost rates may be adjusted from the default values

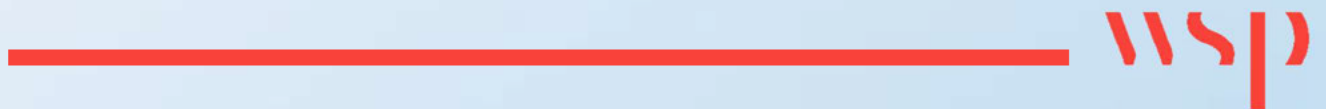
Rate		B&C	M&E	Mains & Sewers	Total
	Standard Cost	£ -	£ -	£ 320,100	£ 320,100
	Non-Standard Cost	£ 266,600	£ -	£ -	£ 266,600
19.3%	Non-Standard Adjustment	£ -	£ -	£ 61,800	£ 61,800
	Construction Cost	£ 266,600	£ -	£ 381,900	£ 648,500
0.0%	Design Fee	£ -	£ -	£ -	£ -
	Contractor D&B Cost	£ 266,600	£ -	£ 381,900	£ 648,500
12.8%	Internal Costs	£ 34,100	£ -	£ 48,800	£ 82,900
18.1%	External Costs	£ 48,200	£ -	£ 69,000	£ 117,200
	Project Total	£ 348,900	£ -	£ 499,700	£ 848,600
31.5%	Optimism Bias	£ 109,900	£ -	£ 157,400	£ 267,300
	Business Case Cost Estimate	£ 458,800	£ -	£ 657,100	£ 1,115,900

These rates and notes may be adjusted from the standard rates
 Costs are calculated using a formula of $M \times (\text{Quantity})^P + C$
 M is a multiplier adjuster, P is a power adjuster, C is a constant
 For Linear Cost Curves set $P = 1$
 For Unit Rate Items set $P = 1, C = 0$

Level 1	Level 2	Level 3	Level 4	Units	B&C					M&E					Mains and Sewers					Notes
					M	P	C	Quantity	Cost	M	P	C	Quantity	Cost	M	P	C	Quantity	Cost	
INFRA	Distribution	Pressure Mains in Field / Verges	Diameter: 700mm	m					£ -						772	1	11,113	400 m	£ 320,094	
NON-STANDARD	PERMANENT SITE WORKS	ACCESS	Access Track	m	4,137	1	0	50 m	£ 43,260	0		0	m	#VALUE!					£ -	
NON-STANDARD	PERMANENT SITE WORKS	PERMANENT SITE FEATURES	Security fencing	m	78	1	0	300 m	£ 23,337					£ -					£ -	
FREE ENTRY	ITEM DESCRIPTION	ITEM UNITS	OTHER DETAILS		100,000	#N/A	#N/A	1	£ 100,000		#N/A	#N/A	1	#VALUE!					£ -	Eel Weir Chamber and Flow Metering
FREE ENTRY	Outlet	ITEM UNITS	OTHER DETAILS		100,000	#N/A	#N/A	1	£ 100,000		#N/A	#N/A		#VALUE!		#N/A	#N/A		#VALUE!	Submerged Outlet

Appendix B

ACWG TEMPLATE FOR OB AND QCRA



3a. Quantitative Costed Risk Assessment - Register Tab

Option Name	Netheridge SRO - Haw Bridge
Option Reference	Option 2
Date of QCRA Review	25.7.22

Score - Description	Max Cost
1 - Very Low	983 933
2 - Low	1 967 870
3 - Medium	4 919 675
4 - High	14 759 023
5 - Very High	29 518 050

Capex: 98 393 500 Insert total scheme capex excluding optimism bias

Risk (static) values:	
P10	7 731 351.65 Insert output from @risk report for 10 percentile
P50	19 122 964.60 Insert output from @risk report for 50 percentile
P90	32 677 017.83 Insert output from @risk report for 90 percentile

Insert Risk ID	Describe nature of risk including cause and event	Describe consequences if risk is realised	Calculated based on Quant Prob %	Insert score	Insert score	Calculated risk score	Insert probability as percentage that risk occurs	Cost Estimates			Risk	Insert specific risk response actions i.e. the steps required to mitigate the risk	Set by default to the pre-mitigation value. However can overwrite to record the anticipated probability of the risk occurring if identified risk response actions are successful	Should be set by default to the pre-mitigation value. However can overwrite to record the anticipated minimum cost impact if identified risk response actions are successful	Should be set by default to the pre-mitigation value. However can overwrite to record the anticipated maximum cost impact if identified risk response actions are successful	Should be set by default to the pre-mitigation value. However can overwrite to record the anticipated maximum cost impact if identified risk response actions are successful
								Min £	MLE	Max £						
Netheridge WwTW Influent Volume	Inadequate flow into Netheridge WwTW during dry weather flow to supply 35 ML/d	STS SRO unable to supply required volume to STT SRO scheme	1	4	2	15%				See Tab 3b.	Storage tank to buffer flows over 24 hour period					See Tab 3b.
Netheridge WwTW Influent Quality	Quality of the influent into Netheridge WwTW changes/deteriorates	New treatment process does not meet STS SRO discharge permit standards. Process upgrades required.				0					Cannot quantify potential 'deterioration' so cannot quantify to action or cost		0%			
Upgrade at Netheridge	Upgrade occur at Netheridge WwTW that utilise existing land power water sludge resources assumed to be available for the SRO scheme	Redesign of proposed new treatment layout. Additional power and water required to site.				0					Cannot quantify to action or cost		0%			
STS SRO Discharge Permit Requirements	Water quality standards for the STS SRO discharge are higher than anticipated	New treatment process does not meet STS SRO discharge permit standards. Process upgrades required.	1	4	2	25%					Increase Options 1 2 3 to Option 4 treatment process		25%			
STS SRO Treatment Process Effluent Quality	The new STS SRO treatment process does not produce effluent to the quality anticipated at design stage	New treatment process does not meet STS SRO discharge permit standards. Process upgrades required.	1	4	2	40%					Increase Options 1 2 3 to Option 4 treatment process.		40%			
STS SRO Treatment Process Layout at WwTW	Specified treatment process units do not fit with proposed WwTW layout requiring redesign	Additional pipework and ancillaries required due to altered layout.	1	1	1	15%					Assume additional 20% pipework required.		15%			
Netheridge WwTW Power Upgrade	Specific treatment process units required additional power requiring additional electrical upgrades	Additional substation/electrical equipment required.	1	2	2	50%					Assume 20% more road/hardstand/drainage etc		50%			
Netheridge WwTW Potable Water Upgrade	Specific treatment process units required additional potable water requiring upgrade to incoming water supply	Upgrade to incoming water supply to increase volume of water supplied	1	1	1	70%					Upgrade to incoming water supply pipeline - study required		70%			
Landownership/Wayleaves	Issues relating to landownership wayleaves and access.	Alteration of pipe route delay to construction or different construction methods				0					Cannot quantify to action or cost		0%			
Planning Permission	Issues relating to obtaining planning permissions for WwTW or pipeline buildings and structures	Alteration of building/structure size/location different construction methods				0					Cannot quantify to action or cost		0%			
Environmental Permits (Ainey)?	Options 1 2 and 3 must pass through Ainey Nature Reserve at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required. Additional mitigation and reinstatement required.	1	2	2	40%					Assume additional cost for micro tunnel OR double reinstatement rate		40%			
Pipe line - Rail Crossing	Options 1 and 2 must pass under the railway at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required.	1	4	2	40%							40%			
Pipe line - Road Crossing	Options 1 2 and 3 must pass under the A40 at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required.	1	1	1	30%							30%			
Pipe line - River Crossing	Options 1 2 and 3 must pass under East Channe R Severn at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required.	1	1	1	30%							30%			
Pipe line - Utilities Diversions	Options 1 2 and 3 must pass through semi rural and urban areas. Pipeline route could uncover unknown services/utilities	Services require diversion or pipe route altered to avoid service/utility.	2	2	1	60%					Assume an additional % for additional service diversions		60%			
Pipe line - Contaminated Land	Options 1 2 and 3 must pass through old landfill site at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative route required increasing pipeline length. Alternative construction methods required.	2	2	1	40%							40%			
Pipe line - Contaminated Land	Options 1 2 and 3 must pass through old railway siding at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative route required increasing pipeline length. Alternative construction methods required.	1	1	1	30%							30%			
Pipe line Ground Water	Options 1 2 and 3 must pass close to R Severn and East Channel R Severn. Trench excavation could experience excessive groundwater ingress.	Alternative construction method or dewatering method required.	2	3	2	60%							60%			
Pipe line Drainage Points	Options 1 2 and 3 require drainage points along the route to allow the pie to be drained when not in use. Permissions have not been granted.	Pipeline could not be drained when not in use leading to operational issues. Alternative pipeline route required to accommodate less tie drain points.	1	3	2	45%							45%			
BLANK ROW - insert rows above to add risks	BLANK ROW - insert rows above to add risks		1	1	1	0%							0%			

3a. Quantitative Costed Risk Assessment - Register Tab

Option Name	Netheridge SRO - East Channel
Option Reference	Option 3
Date of QCRA Review	26/07/2022

Score - Description	Max Cost
1 - Very Low	
2 - Low	
3 - Medium	
4 - High	
5 - Very High	

Capex: [redacted] Insert total scheme capex excluding optimism bias

Risk (static values):

P10: [redacted] Insert output from @risk report for 10 percentile

P50: [redacted] Insert output from @risk report for 50 percentile

P90: [redacted] Insert output from @risk report for 90 percentile

Insert Risk ID	Describe nature of risk including cause and event	Describe consequences if risk is realised	Calculated based on Quant Prob %	Insert score	Insert score	Calculated risk score	Insert probability as percentage that risk occurs	Cost Estimates			Risk	Insert specific risk response actions i.e. the steps required to mitigate the risk	Set by default to the pre-mitigation value. However can overwrite to record the anticipated probability of the risk occurring if identified risk response actions are successful	Should be set by default to the pre-mitigation value. However can overwrite to record the anticipated minimum cost impact if identified risk response actions are successful	Should be set by default to the pre-mitigation value. However can overwrite to record the anticipated maximum cost impact if identified risk response actions are successful	Not used on Tab 3a - see Tab 3b
								Min £	MLE	Max £						
Netheridge WwTW Influent Volume	Inadequate flow into Netheridge WwTW during dry weather flow to supply 35 Ml/d	STS SRO unable to supply required volume to STS SRO scheme	1	4	2	15%				See Tab 3b.	Storage tank to buffer flows over 24 hour period				See Tab 3b.	
Netheridge WwTW Influent Quality	Quality of the influent into Netheridge WwTW changes/deteriorates	New treatment process does not meet STS SRO discharge permit standards. Process upgrades required.				0					Cannot quantify potential 'deterioration' so cannot quantify to action or cost		0%			
Upgrade of Netheridge WwTW	Upgrade occur at Netheridge WwTW that utilise existing land power water sludge resources assumed to be available for the SRO scheme	Redesign of proposed new treatment layout. Additional power and water required to site.				0					Cannot quantify to action or cost		0%			
STS SRO Discharge Permit Requirements	Water quality standards for the STS SRO discharge are higher than anticipated	New treatment process does not meet STS SRO discharge permit standards. Process upgrades required.	1	4	2	25%					Increase Options 1 2 3 to Option 4 treatment process		25%			
STS SRO Treatment Process Effluent Quality	The new STS SRO treatment process does not produce effluent to the quality anticipated at design stage	New treatment process does not meet STS SRO discharge permit standards. Process upgrades required.	1	4	2	40%					Increase Options 1 2 3 to Option 4 treatment process.		40%			
STS SRO Treatment Process Layout at WwTW	Specified treatment process units do not fit with proposed WwTW layout requiring redesign	Additional pipework and ancillaries required due to altered layout.	1	1	1	15%					Assume additional 20% pipework required.		15%			
Netheridge WwTW Power Upgrade	Specific treatment process units required additional power requiring additional electrical upgrades	Additional substation/electrical equipment required.	1	2	2	50%					Assume 20% more road/hardstand/drainage etc. Engagement with power supplier required.		50%			
Netheridge WwTW Potable Water Upgrade	Specific treatment process units required additional potable water requiring upgrade to incoming water supply	Upgrade to incoming water supply to increase volume of water supplied	1	1	1	70%					Upgrade to incoming water supply pipeline - study required		70%			
Landownership/Wayleaves	Issues relating to landownership wayleaves and access.	Alteration of pipe route delay to construction or different construction methods				0					Cannot quantify to action or cost		0%			
Planning Permission	Issues relating to obtaining planning permissions for WwTW or pipeline buildings and structures	Alteration of building/structure size/location different construction methods				0					Cannot quantify to action or cost		0%			
Environmental Permits (Ainey)?	Options 1 2 and 3 must pass through Ainey Nature Reserve at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required. Additional mitigation and reinstatement required.	1	2	2	15%					Assume additional cost for micro tunnel OR double reinstatement rate		15%			
Pipe line - Rail Crossing	Options 1 and 2 must pass under the railway at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required.														
Pipe line - Road Crossing	Options 1 2 and 3 must pass under the A40 at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required.														
Pipe line - River Crossing	Options 1 2 and 3 must pass under East Channe R Severn at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required.	1	1	1	30%							30%			
Pipe line - Utilities Diversions	Options 1 2 and 3 must pass through semi rural and urban areas. Pipeline route could uncover unknown services/utilities	Services require diversion or pipe route altered to avoid service/utility.	2	2	1	50%					Assume an additional % for additional service diversions		50%			
Pipe line - Contaminated Land	Options 1 2 and 3 must pass through old landfill site at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative route required increasing pipeline length. Alternative construction methods required.	2	2	1	40%							40%			
Pipe line - Contaminated Land	Options 1 2 and 3 must pass through old railway siding at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative route required increasing pipeline length. Alternative construction methods required.	1	1	1	15%							15%			
Pipe line Ground Water	Options 1 2 and 3 must pass close to R Severn and East Channel R Severn. Trench excavation could experience excessive groundwater ingress.	Alternative construction method or dewatering method required.	2	3	2	45%							45%			
Pipe line Drainage Points	Options 1 2 and 3 require drainage points along the route to allow the pie to be drained when not in use. Permissions have not been granted.	Pipeline could not be drained when not in use leading to operational issues. Alternative pipeline route required to accommodate less tie drain points.	1	3	2	30%							30%			
BLANK ROW - insert rows above to add risks	BLANK ROW - insert rows above to add risks		1	1	1	#VALUE!							0%			

3a. Quantitative Costed Risk Assessment - Register Tab

Option Name	Netheridge SRO - East Channel SW Branch
Option Reference	Option 5
Date of QCRA Review	30.05.21

Score - Description	Max Cost
1 - Very Low	92 908
2 - Low	183 816
3 - Medium	464 340
4 - High	1 393 620
5 - Very High	2 787 240

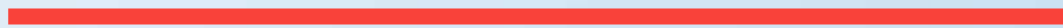
Capex: [redacted] Insert total scheme capex excluding optimism bias

Risk (static values):
 P10 [redacted] Insert output from @risk report for 10 percentile
 P50 [redacted] Insert output from @risk report for 50 percentile
 P90 [redacted] Insert output from @risk report for 90 percentile

Insert Risk ID	Describe nature of risk including cause and event	Describe consequences if risk is realised	Calculated based on Quant Prob %	Insert score	Insert score	Calculated risk score	Insert probability as percentage that risk occurs	Cost Estimates			Risk	Insert specific risk response actions i.e. the steps required to mitigate the risk	Set by default to the pre-mitigation value. However can overwrite to record the anticipated probability of the risk occurring if identified risk response actions are successful	Should be set by default to the pre-mitigation value. However can overwrite to record the anticipated minimum cost impact if identified risk response actions are successful	Should be set by default to the pre-mitigation value. However can overwrite to record the anticipated maximum cost impact if identified risk response actions are successful	Not used on Tab 3a - see Tab 3b
								Min £	MLE	Max £						
Netheridge WwTW Influent Volume	Inadequate flow into Netheridge WwTW during dry weather flow to supply 35 ML/d	STS SRO unable to supply required volume to STS SRO scheme	1	4	2	15%				See Tab 3b.	Storage tank to buffer flows over 24 hour period				See Tab 3b.	
Netheridge WwTW Influent Quality	Quality of the influent into Netheridge WwTW changes/deteriorates	New treatment process does not meet STS SRO discharge permit standards. Process upgrades required.				0					Cannot quantify potential 'deterioration' so cannot quantify to action or cost		0%			
Upgrade of Netheridge WwTW	Upgrade occur at Netheridge WwTW that utilise existing land power water studge resources assumed to be available for the SRO scheme	Redesign of proposed new treatment layout. Additional power and water required to site.				0					Cannot quantify to action or cost		0%			
STS SRO Discharge Permit Requirements	Water quality standards for the STS SRO discharge are higher than anticipated	New treatment process does not meet STS SRO discharge permit standards. Process upgrades required.	1	4	2	25%					Increase Options 1 2 3 to Option 4 treatment process		25%			
STS SRO Treatment Process Effluent Quality	The new STS SRO treatment process does not produce effluent to the quality anticipated at design stage	New treatment process does not meet STS SRO discharge permit standards. Process upgrades required.	1	4	2	40%					Increase Options 1 2 3 to Option 4 treatment process.		40%			
STS SRO Treatment Process Layout at WwTW	Specified treatment process units do not fit with proposed WwTW layout requiring redesign	Additional pipework and ancillaries required due to altered layout.	1	1	1	10%					Assume additional 20% pipework required. Assume 20% more road/hardstand/drainage etc. Engagement with power supplier required.		10%			
Netheridge WwTW Power Upgrade	Specific treatment process units required additional power requiring additional electrical upgrades	Additional substation/electrical equipment required.	1	2	2	30%					Engagement with power supplier required.		30%			
Netheridge WwTW Potable Water Upgrade	Specific treatment process units required additional potable water requiring upgrade to incoming water supply	Upgrade to incoming water supply to increase volume of water supplied	1	1	1	30%					Upgrade to incoming water supply pipeline - study required		30%			
Landownership/Wayleaves	Issues relating to landownership wayleaves and access.	Alteration of pipe route delay to construction or different construction methods				0					Cannot quantify to action or cost		0%			
Planning Permission	Issues relating to obtaining planning permissions for WwTW or pipeline buildings and structures	Alteration of building/structure size/location different construction methods				0					Cannot quantify to action or cost		0%			
Environmental Permits (Ainey)?	Options 1 2 and 3 must pass through Ainey Nature Reserve at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required. Additional mitigation and reinstatement required.	1	2	2	25%					Assume additional cost for micro tunnel OR double reinstatement rate		25%			
Pipe line - Rail Crossing	Options 1 and 2 must pass under the railway at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required.														
Pipe line - Road Crossing	Options 1 2 and 3 must pass under the A40 at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required.														
Pipe line - River Crossing	Options 1 2 and 3 must pass under East Channel 8 Severn at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative location required for crossing increasing pipeline length. Alternative construction methods required.	1	1	1	30%							30%			
Pipe line - Utilities Diversions	Options 1 2 and 3 must pass through semi rural and urban areas. Pipeline route could uncover unknown services/utilities	Services require diversion or pipe route altered to avoid service/utility.	2	2	1	40%					Assume an additional % for additional service diversions		40%			
Pipe line - Contaminated Land	Options 1 2 and 3 must pass through old landfill site at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative route required increasing pipeline length. Alternative construction methods required.	2	2	1	40%							40%			
Pipe line - Contaminated Land	Options 1 2 and 3 must pass through old railway siding at Ch.XXX. Permissions have not been granted/ construction methods agreed.	Alternative route required increasing pipeline length. Alternative construction methods required.	1			0							0%			
Pipe line Ground Water	Options 1 2 and 3 must pass close to 8 Severn and East Channel 8 Severn. Trench excavation could experience excessive groundwater ingress.	Alternative construction method or dewatering method required.	2	3	2	6	45%						45%			
Pipe line Drainage Points	Options 1 2 and 3 require drainage points along the route to allow the pie to be drained when not in use. Permissions have not been granted.	Pipeline could not be drained when not in use leading to operational issues. Alternative pipeline route required to accommodate less tie drain points.	1	3	2	20%							20%			
BLANK ROW - insert rows above to add risks	BLANK ROW - insert rows above to add risks		1	1	1	#VALUE!							0%			

Appendix C

OPEX COST ESTIMATES



Netheridge SRO Treatment Plant Operational Cost Estimate (19/10/22) - Option 1

Days pumping per annum
Days pumping sweetening flow
Days on standby
Power Unit Cost (£/kWh)
Operator Cost (£/hr)

Process Equipment	Power Rating (kW)	Power Consumption - Variable					Person Costs - Fixed			Fixed		Average Daily Cost	
		35MLD kWh/d	20MLD - kWh/d	Used during standby?	Daily Cost 35 MLD	Daily Cost 20MLD	Annual Power Cost	Operator Time (days)	Maintenance Time (days)	Annual Person Cost (£/pa)	Consumables Costs (£/pa)		Total Annual Opex Cost
Ferrous Sulphate	1	24	13.68	Yes				16	12				
MBBR Lift Pump Station	150	1456	829.92	Yes				13	3				
MBBR, incl blowers	480	5760	3283.2	Yes				39	3				
CoMag Equipment	16	200	114	Yes				26	10				
Ferric Sulphate	1	24	13.68	Yes				16	12				
Polymer	1	24	13.68	Yes				16	12				
Magnetite		0		Yes				16	1				
Sludge Recycle System		50	28.5	Yes				13	12				
Ozone Pump Station	150	1456	829.92	Yes				13	12				
Ozone Plant Equipment		2562	1460.34	no				26	12				
BAFF Lift PS	150	1456	829.92	Yes				13	12				
BAFF, incl blowers	156	1806	1029.42	Yes				39	12				
Backwash Pumps	69	18.5	10.545	Yes				13	12				
Backwash Return pumps	15	35	19.95	Yes				13	12				
GAC Equipment		43	24.51	no				26	12				
GAC Media		0		no				0	22				
Sodium Hypochlorite	1	24	13.68	Yes				16	12				
Sludge thickener (incl feed pumps)		39	22.23	Yes				13	12				
Thickened Sludge Pumps	8	32	18.24	Yes				13	12				
Pump to Existing Outfall	74	1400	798	Yes				10					
Transfer Pump Station (Pipeline Option 1)	645	7140	4069.8	no				15					

Assuming additional 5% m

Treatment	Total annual	
	Total daily	
Pipeline	Total annual	
	Total daily	
	Rounded combined Total	

CHEMICALS BELOW:

		Daily Cost	Annual Cost
Ferrous Sulphate	yes		
Ferric Sulphate	yes		
Polymer	yes		
Magnetite	yes		
Liquid Oxygen	yes		
Sodium Hypo	yes		
Sludge polymer	yes		

Annual Fixed	
Annual Variable cost	
Variable (£/ML)	

Netheridge SRO Treatment Plant Operational Cost Estimate (19/10/22) - Option 2

Days pumping per annum
Days pumping sweetening flow
Days on standby
Power Unit Cost (£/kWh)
Operator Cost (£/hr)



Process Equipment	Power Rating (kW)	35MLD - kWh/d	20MLD - kWh/d	Used during standby?	Power Costs			Person Costs			Consumables Cost	Total Annual	Average Daily Cost
					Daily Cost 35 MLD	Daily Cost 20MLD	Annual Cost	Operator Time (days)	Maintenance Time (days)	Total Person Cost (£/pa)			
Ferrous Sulphate		1	24	13.68	Yes				16	12			
MBBR Lift Pump Station		150	1456	829.92	Yes				13	3			
MBBR, incl blowers		480	5760	3283.2	Yes				39	3			
CoMag Equipment		16	200	114	Yes				26	10			
Ferric Sulphate		1	24	13.68	Yes				16	12			
Polymer		1	24	13.68	Yes				16	12			
Magnetite			0		Yes				16	1			
Sludge Recycle System			50	28.5	Yes				13	12			
Ozone Pump Station		150	1456	829.92	Yes				13	12			
Ozone Plant Equipment			2562	1460.34	no				26	12			
BAFF Lift PS		150	1456	829.92	Yes				13	12			
BAFF, incl blowers		156	1806	1029.42	Yes				39	12			
Backwash Pumps		69	18.5	10.545	Yes				13	12			
Backwash Return pumps		15	35	19.95	Yes				13	12			
GAC Equipment			43	24.51	no				26	12			
GAC Media			0		no				0	22			
Sodium Hypochlorite		1	24	13.68	Yes				16	12			
Sludge thickener (incl feed pumps)			39	22.23	Yes				13	12			
Thickened Sludge Pumps		8	32	18.24	Yes				13	12			
Pump to Existing Outfall		74	1400	798	Yes				10				
Transfer Pump Station (Pipeline Option 2)		510	4900	2793	no				15				

Assuming €

Treatment	Total annual	
	Total daily	
Pipeline	Total annual	
	Total daily	
	Rounded	
	Combined Total	

CHEMICALS BELOW:

		Daily Cost	Annual Cost
Ferrous Sulphate	yes		
Ferric Sulphate	yes		
Polymer	yes		
Magnetite	yes		
Liquid Oxygen	yes		
Sodium Hypo	yes		
Sludge Polymer	yes		

Annual Fixed	
Annual Variable cost	
Variable (£/ML)	

Netheridge SRO Treatment Plant Operational Cost Estimate (19/10/22) - Option 3

Days pumping per annum
Days pumping sweetening flow
Days on standby
Power Unit Cost (£/kWh)
Operator Cost (£/hr)



Process Equipment	Power Rating (kW)	35MLD - kWh/d	20MLD - kWh/d	Used during standby?	Power Costs			Person Costs			Consumables Costs (£/pa)	Total Annual	Average Daily Cost
					Daily Cost 35 MLD	Daily Cost 20MLD	Annual Cost	Operator Time (days)	Maintenance Time (days)	Total Person Cost (£/pa)			
Ferrous Sulphate		1	24	13.68	Yes				16	12			
MBBR Lift Pump Station		150	1456	829.92	Yes				13	3			
MBBR, incl blowers		480	5760	3283.2	Yes				39	3			
CoMag Equipment		16	200	114	Yes				26	10			
Ferric Sulphate		1	24	13.68	Yes				16	12			
Polymer		1	24	13.68	Yes				16	12			
Magnetite			0		Yes				16	1			
Sludge Recycle System			50	28.5	Yes				13	12			
Ozone Pump Station		150	1456	829.92	Yes				13	12			
Ozone Plant Equipment			2562	1460.34	no				26	12			
BAFF Lift PS		150	1456	829.92	Yes				13	12			
BAFF, incl blowers		156	1806	1029.42	Yes				39	12			
Backwash Pumps		69	18.5	10.545	Yes				13	12			
Backwash Return pumps		15	35	19.95	Yes				13	12			
GAC Equipment			43	24.51	no				26	12			
GAC Media			0		no				0	22			
Sodium Hypochlorite		1	24	13.68	Yes				16	12			
Sludge thickener (incl feed pump)		16	39	22.23	Yes				13	12			
Thickened Sludge Pumps		8	32	18.24	Yes				13	12			
Ion Exchange Pump Station		150	1456	829.92	no				13	3			
Ion Exchange			0	0	no				13	12			
Pump to Existing Outfall		74	1400	798	Yes				10				
Transfer Pump Station (Pipeline Option 3)		135	1120	638.4	no				5				

Assuming €

Treatment	Total annual	
	Total daily	
Pipeline	Total annual	
	Total daily	
	Rounded Combined Total	

CHEMICALS BELOW:

		Daily Cost	Annual Cost	Annual Fixed	Annual Variable cost	Variable (£/ML)
Ferrous Sulphate	yes					
Ferric Sulphate	yes					
Polymer	yes					
Magnetite	yes					
Liquid Oxygen	yes					
Sodium Hypo	yes					
Sludge Polymer	yes					

Netheridge SRO Treatment Plant Operational Cost Estimate (19/10/22) - Option 4

Days pumping per annum
Days pumping sweetening flow
Days on standby
Power Unit Cost (£/kWh)
Operator Cost (£/hr)

Process Equipment	Power Rating (kW)	35MLD - kWh/d	20MLD - kWh/d	Used during standby?	Power Costs			Person Costs			Consumables Costs (£/pa)	Total Annual	Average Daily Cost
					Daily Cost 35 MLD	Daily Cost 20MLD	Annual Cost	Operator Time (days)	Maintenance Time (days)	Total Person Cost (£/pa)			
Ferrous Sulphate		1	24	13.68	Yes				16	12			
MBBR Lift Pump Station		150	1456	829.92	Yes				13	3			
MBBR, incl blowers		480	5760	3283.2	Yes				39	3			
CoMag Equipment		16	200	114	Yes				26	10			
Ferric Sulphate		1	24	13.68	Yes				16	12			
Polymer		1	24	13.68	Yes				16	12			
Magnetite			0		Yes				16	1			
Sludge Recycle System			50	28.5	Yes				13	12			
Ozone Pump Station		150	1456	829.92	Yes				13	12			
Ozone Plant Equipment			2562	1460.34	no				26	12			
BAFF Lift PS		150	1456	829.92	Yes				13	12			
BAFF, incl blowers		156	1806	1029.42	Yes				39	12			
Backwash Pumps		69	18.5	10.545	Yes				13	12			
Backwash Return pumps		15	35	19.95	Yes				13	12			
GAC Equipment			43	24.51	no				26	12			
GAC Media			0		yes				0	22			
Sodium Hypochlorite		1	24	13.68	Yes				16	12			
Sludge thickener (incl feed pump)		16	39	22.23	Yes				13	12			
Thickened Sludge Pumps		8	32	18.24	Yes				13	12			
Ion Exchange Pump Station		150	1456	829.92	no				13	3			
Ion Exchange				0	no				13	12			
UV		44	684	389.88	no				13	12			
Pump to Existing Outfall		74	1400	798	Yes				10				
Transfer Pump Station (Pipeline Option 4)		135	1225	698.25	no				5				

Assuming €

Treatment	Total annual	
	Total daily	
Pipeline	Total annual	
	Total daily	
	Rounded Combined Total	

CHEMICALS BELOW:

		Daily Cost	Annual Cost
Ferrous Sulphate	yes		
Ferric Sulphate	yes		
Polymer	yes		
Magnetite	yes		
Liquid Oxygen	yes		
Sodium Hypo	yes		
Sludge Polymer	yes		

Annual Fixed	
Annual Variable cost	
Variable (£/ML)	

Netheridge SRO Treatment Plant Operational Cost Estimate (19/10/22) - Option 5

Days pumping per annum	
Days pumping sweetening flow	
Days on standby	
Power Unit Cost (£/kWh)	
Operator Cost (£/hr)	

Process Equipment	35MLD - kWh/d	20MLD - kWh/d	Used during standby?	Power Costs			Person Costs			Consumables Costs (£/pa)	Total Annual	Average Daily Cost
				Daily Cost 35 MLD	Daily Cost 20MLD	Annual Cost	Operator Time (days)	Maintenance Time (days)	Total Person Cost (£/pa)			
Ferrous Sulphate	24	13.68	Yes				16	12				
MBBR Lift Pump Station	1456	829.92	Yes				13	3				
MBBR, incl blowers	5760	3283.2	Yes				39	3				
CoMag Equipment	200	114	Yes				26	10				
Ferric Sulphate	24	13.68	Yes				16	12				
Polymer	24	13.68	Yes				16	12				
Magnetite	0		Yes				16	1				
Sludge Recycle System	50	28.5	Yes				13	12				
Ozone Pump Station	1456	829.92	Yes				13	12				
Ozone Plant Equipment	2562	1460.34	no				26	12				
BAFF Lift PS	1456	829.92	Yes				13	12				
BAFF, incl blowers	1806	1029.42	Yes				39	12				
Backwash Pumps	18.5	10.545	Yes				13	12				
Backwash Return pumps	35	19.95	Yes				13	12				
GAC Equipment	43	24.51	no				26	12				
GAC Media	0		no				0	22				
Sodium Hypochlorite	24	13.68	Yes				16	12				
Sludge thickener (incl feed pump)	39	22.23	Yes				13	12				
Thickened Sludge Pumps	32	18.24	Yes				13	12				
Ion Exchange Pump Station	1456	829.92	no				13	3				
Ion Exchange	0	0	no				13	12				
Pump to Existing Outfall	1400	798	Yes				10					
Transfer Pump Station (Pipeline Option 2)	4900	2793	no				15					
Transfer Pump Station (Pipeline Option 3)	1120	638.4	no				5					

Assuming a

Full system		
Treatment	Total annual	
	Total daily	
Pipeline	Total annual	
	Total daily	
	Rounded	
	Combined Total	

CHEMICALS BELOW:

	Daily Cost	Annual Cost
Ferrous Sulphate		
Ferric Sulphate		
Polymer		
Magnetite		
Liquid Oxygen		
Sodium Hypo		
Sludge Polymer		

Annual Fixed	
Annual Variable cost	
Variable (£/ML)	



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